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~~Sub-sonic Flare  
Stack Sizing~~

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*module to*

*process text*

*files part1*

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~~EP 03 17th~~

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~~Oct 2019 — HAR~~

~~PAL GEO ++~~

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*Tum Ho Episode 8*

*/ 5th October*

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*Digital*

*[Subtitle Eng]*

Selection and

Sizing of

Pressure Relief

Valves Regular

Expressions in

*Page 10/94*

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Beginners |  
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Live - 1 How do  
we Improve Our  
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~~Application~~

~~Runtime~~

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2270-30BCE |  
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Enhance Valve  
Change-outs,  
Minimizing  
Downtime ~~Closing  
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ANSI/API

STANDARD 521

FIFTH EDITION,

JANUARY 2007 ISO

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and Depressuring  
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5.15.7.4 Liquid  
cooling service

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and ...~~

Api 521 5th  
*Page 19/94*

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should be more  
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ssure-relieving  
and Depressuring  
Systems, is  
perhaps the most  
thorough  
published

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guidelines on how to size relief devices and flare systems. This paper reviews the differences between the 6thEdition of API STD 521 (Published in 2014) and the 5thedition (Published in



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2007) .

~~Abstract:~~

~~Changes Between  
API STD 521 6th  
Ed and 5th Ed~~

~~...~~

“Control Valve  
Handbook”,  
Emerson’s  
Fisher’s  
Handbook, 5th  
Edition 3.

“Pressure

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Relieving and  
Depressuring  
Systems", API  
Standard 521,  
6th Edition,  
January 2014 4.  
"API 521 7th  
Edition Ballot  
Item 6.4 Work  
Item 30 -  
Thermal  
Expansion  
Equation  
Definitions" 5.

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~~Pressure Safety  
Valve (PSV)  
Sizing Tutorial  
— API~~

~~520/521/526~~

Pressure-  
Relieving and  
Depressuring  
Systems, API  
Standard 521,  
Fifth Edition,  
January 2007 and  
Addendum, May

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2008. Author.

Peter Cain is a  
process  
consultant for  
Petrobras in  
Brazil (Phone: 5  
5-21-98211-0627;  
Email: petercain  
@rocketmail.com)  
. He has more  
than 40 years of  
experience in  
positions  
including

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process  
engineer, job  
leader,  
technical ...

~~Optimizing  
Pressure Relief  
Systems—  
Chemical  
Engineering ...~~

In the API 521  
(fifth edition,  
para 5.14.4.1),  
there is a

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formula to  
calculate the  
final pressure  
of trapped  
liquid for  
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expansion case.  
I have two  
questions; I  
want to use this  
formula and  
justify that for  
my case,  
athermal relief

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valve is not required due to huge difference between maximum operating pressure (3.5 barg) and design pressure (100 barg) of pipe.

~~Thermal  
Expansion, Final  
Pressure  
Relief Devices~~

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~~Forum ...~~

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Pressure-

relieving and

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Systems SIXTH

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C52106 This

standard is

applicable to pr



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essure-relieving  
and vapor  
depressuring  
systems.

Although  
intended for use  
primarily in oil  
refineries, it  
is also  
applicable to  
petrochemical

~~API Standard 521~~

Emergency

*Page 33/94*

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depressuring. In 1997, the American Petroleum Institute published the 4th edition of API 521, Guide for Pressure Relieving and Emergency Depressuring. The most recent version is

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equivalent to  
ISO 23251. Even  
so, one can  
still find  
differences in  
emergency  
depressuring  
(EDP) systems.  
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information,  
please review  
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~~Depressuring  
Systems — an  
overview —  
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Topics~~

API STD 521, 7th  
Edition, June  
2020 - Pressure-  
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and vapor  
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Although  
intended for use  
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applicable to  
petrochemical  
facilities, gas  
plants,  
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- Pressure  
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...

API 521, 5th Edition, does not currently provide specific recommendations for maximum velocities for tail pipes and flare headers, although many companies have such standards. This topic will



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be considered  
for the next  
edition of the  
standard.

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and ...~~

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Item 6.4 Work  
Item 30 -  
Thermal

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Expansion

Equation

Definitions

Background Work

Item 30: #

Source Section

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4.4.12 Clarify /  
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pressure in  
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rationales, and  
case studies.

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guide for Layers  
of Protection

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riskreductions  
accomplished  
through non-SIS  
alternatives; i.  
e.administrative  
procedures,  
equipment  
design, etc.  
Itaddresses  
issues such as  
how to ensure  
the  
effectiveness



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controls  
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Maintenance, and  
Emergency  
Response relate  
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eliminates a  
scenario or

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fundamentally  
reduces a hazard  
Preventive/Proac  
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such as enhanced  
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stops chain of  
events after  
initiating event  
occurs but  
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incident has occurred such as high level in a tank shutting off the pump.

Mitigation (active or passive)

minimizes impact once an incident has occurred such as closing block valves once LEL

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(active) or the  
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responsibilities  
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*Page 64/94*



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understanding  
problems of fire

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and gas-  
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systems, alarm  
systems, and  
methods of fire  
suppression. The

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essential  
reference tool  
for engineers,  
designers and  
others facing  
fire protection  
issues Based on  
the latest NFPA  
standards and  
interpretations

The Instrument

*Page 72/94*



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Handbook (IAEH)  
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available on  
fire protection  
and prevention  
in chemical  
petrochemical

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Ingredient (API)

*Page 85/94*

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to market, many steps must be followed to ensure compliance with governmental regulations.

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of the  
preparation and  
use of APIs  
globally. Topics  
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no "perfect"  
solution or  
absolute zero  
risk,

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Design Solutions  
to Process  
Equipment  
Failures,  
industry experts  
offer their  
broad experience



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numerous  
solutions to the  
more common  
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procedural  
solutions, in  
decreasing order

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of robustness  
and reliability.  
The book  
challenges the  
engineer to  
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opportunities  
for inherent and  
passive safety  
features early,  
and use a risk-  
based approach  
to process  
safety systems

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making risk-  
based design  
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potential  
failure  
scenarios for 10  
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categories; and  
3) two worked  
examples showing  
how the  
techniques can  
be applied. The  
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categories  
covered are:  
vessels,  
reactors, mass  
transfer  
equipment, fluid  
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